

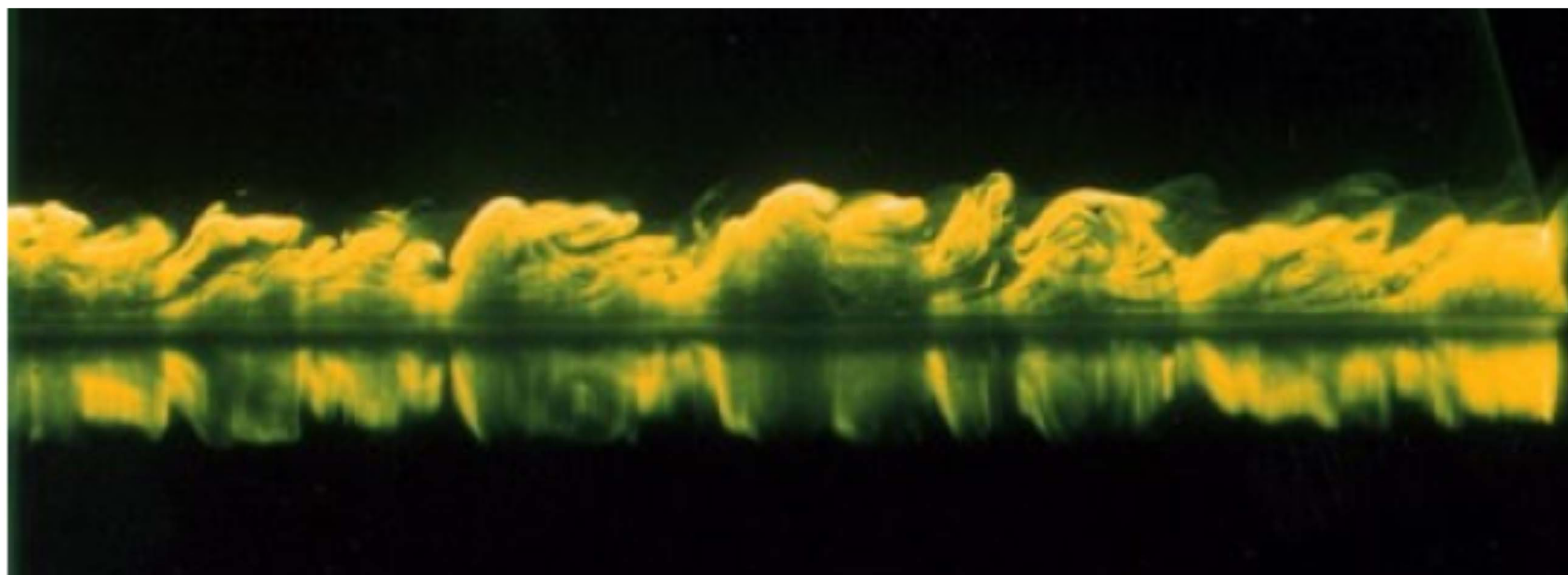


Turbulence

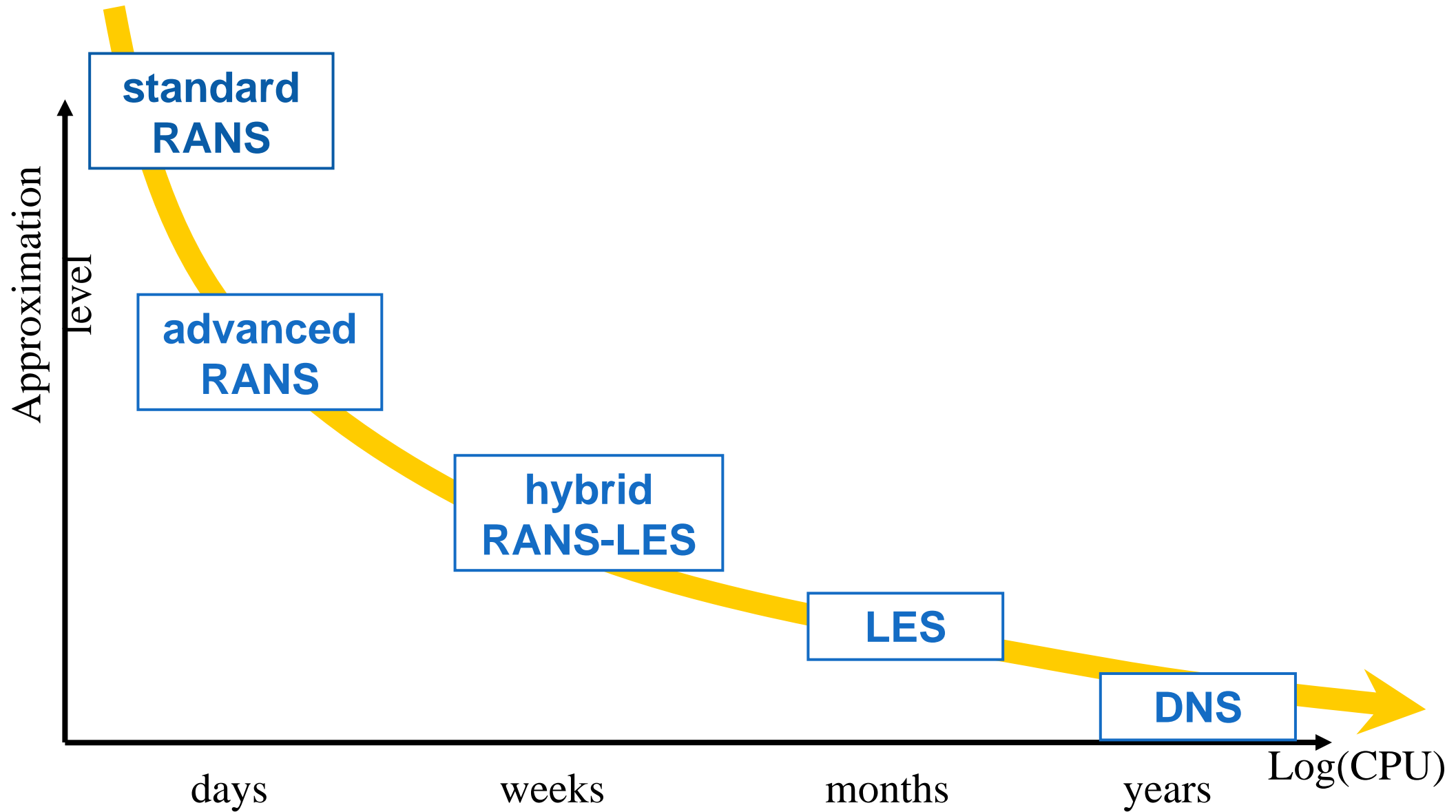
There are no “simple” turbulent flows

Turbulent boundary layer:

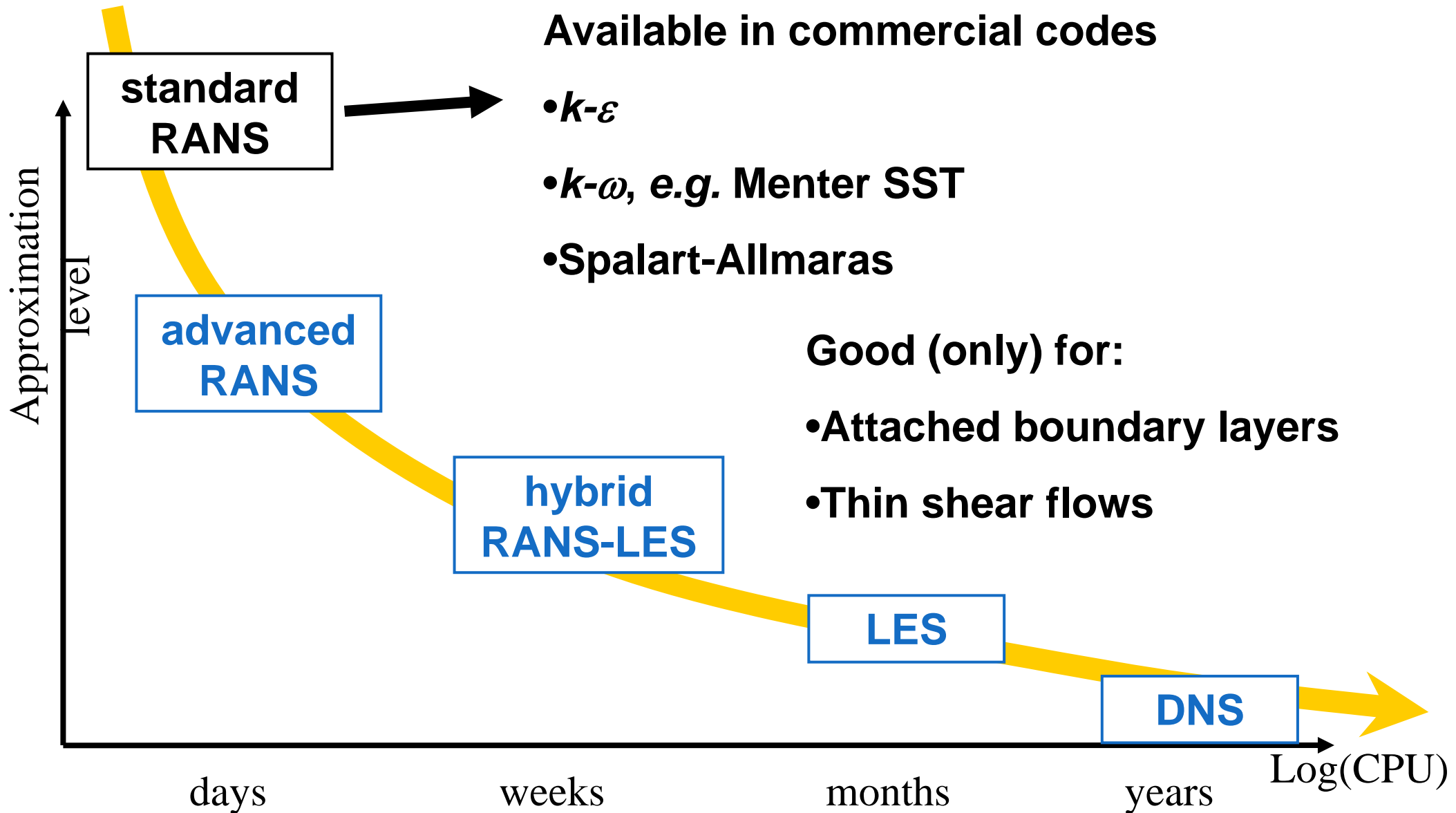
- Instantaneous velocity field (snapshot) $u_i(\mathbf{x}, t)$



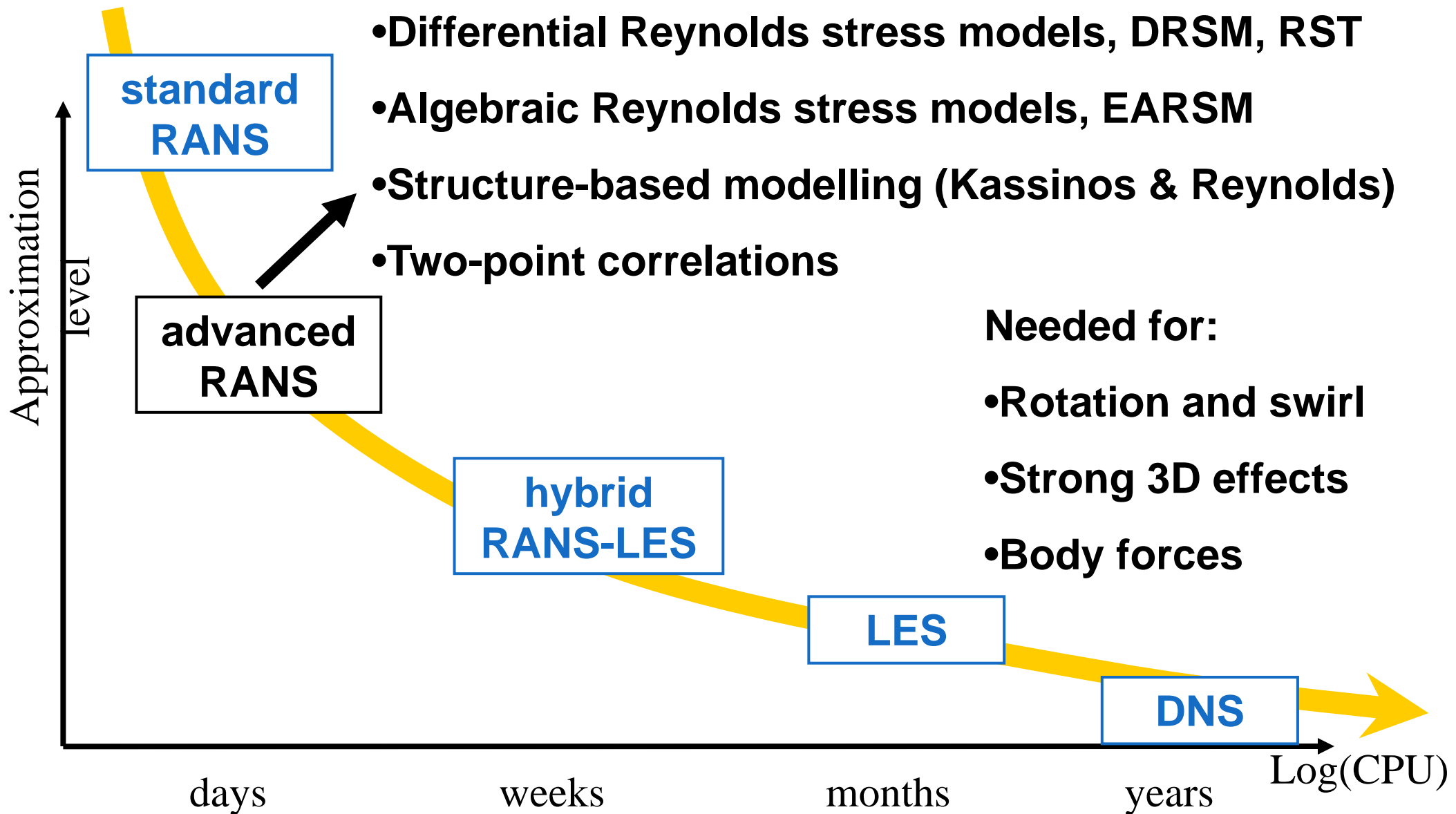
Prediction of turbulent flows



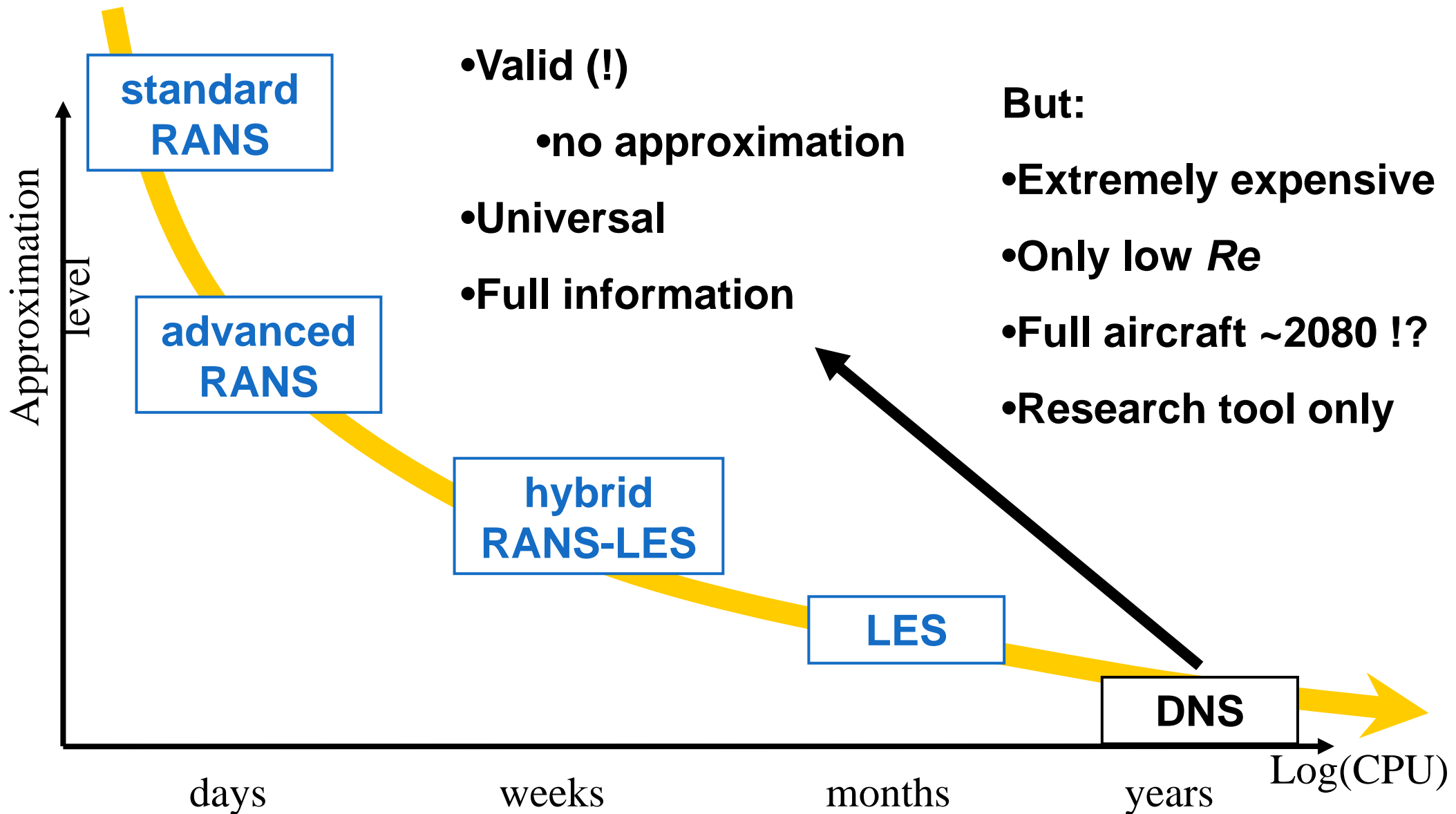
Standard RANS models



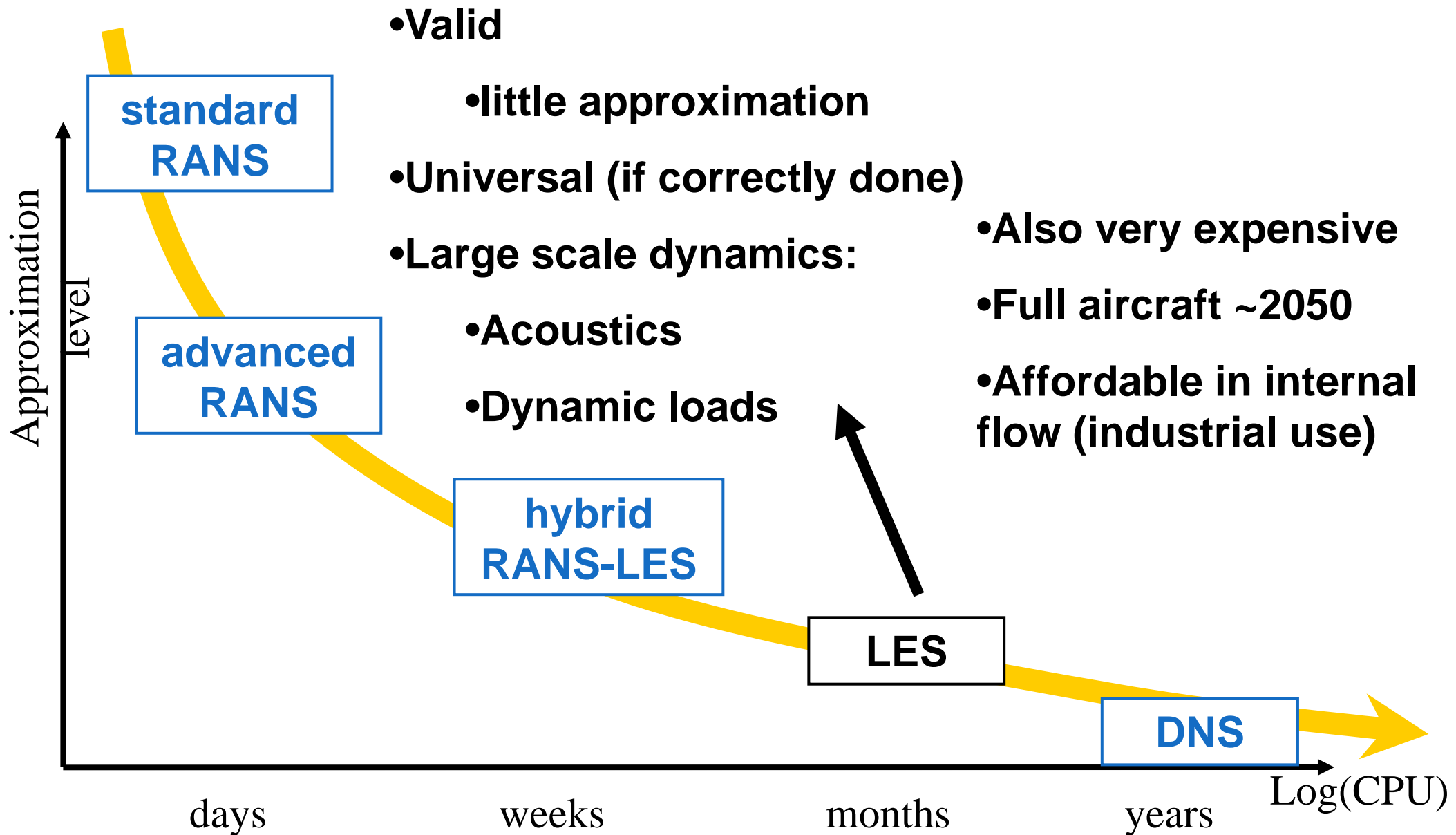
Advanced RANS models



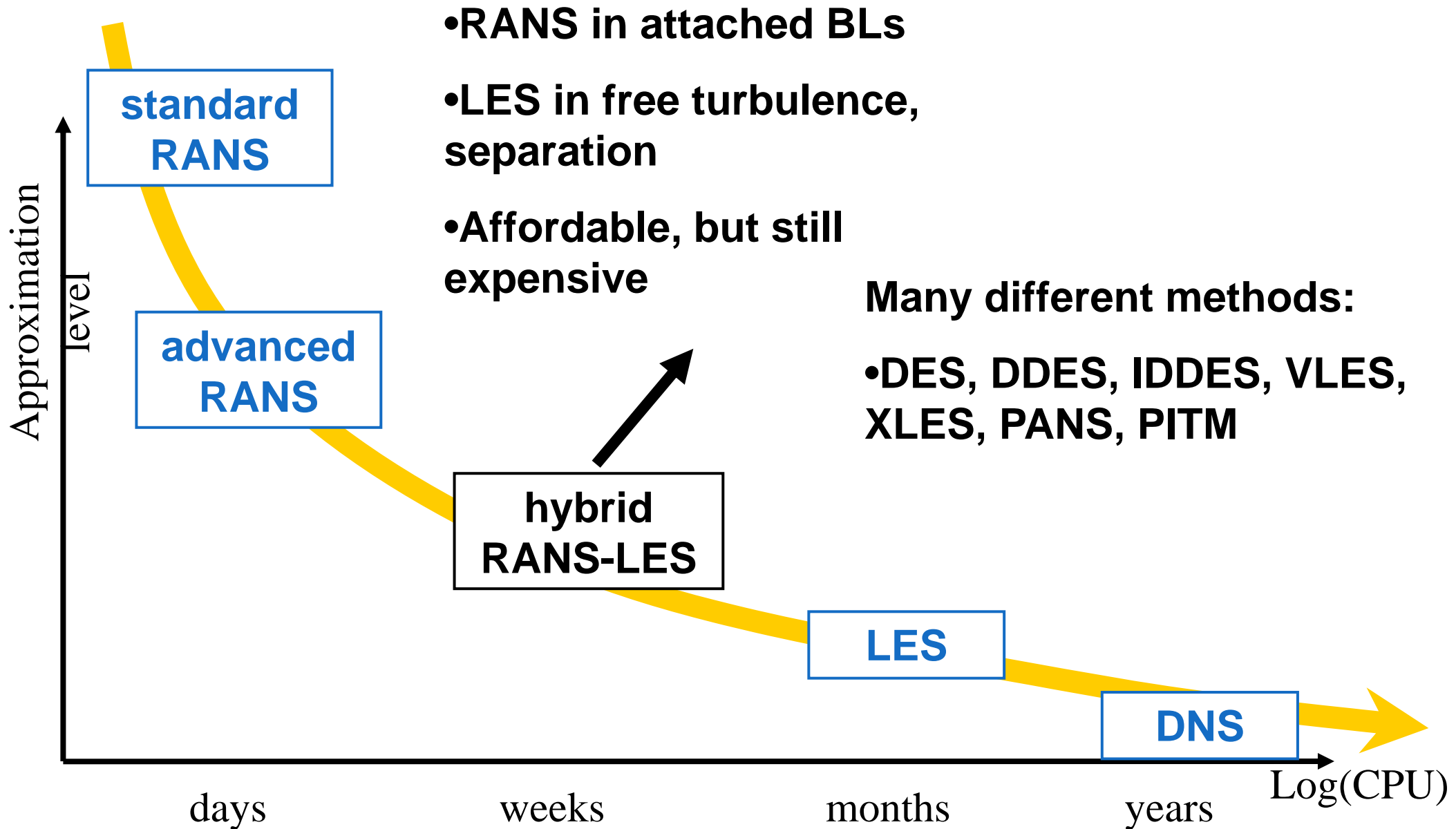
Direct Numerical Simulation – DNS



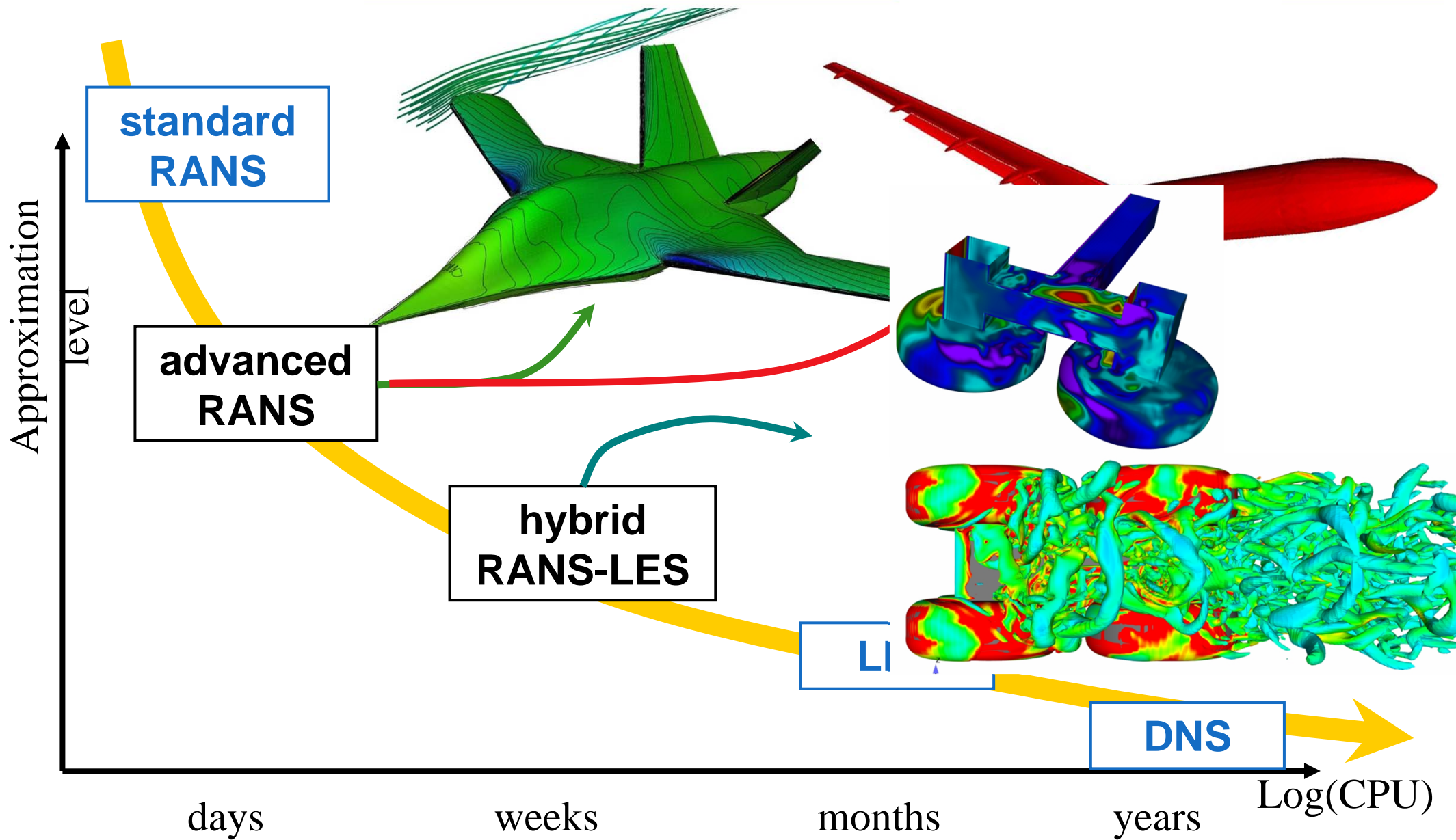
Large Eddy Simulation – LES



Hybrid RANS – LES methods



Prediction of turbulent flows



Basic concepts



- Turbulence is:
 - random fluctuations
 - 3D
 - time dependent
 - present in most flows of engineering interest
- Energy cascade
 - generated at the largest scales (L and U)
 - large scale vortices break down to smaller vortices
 - dissipates to heat at the smallest viscous scales, ε
 - balanced cascade

$$\varepsilon \sim \frac{U^3}{L}$$

- turbulent kinetic energy

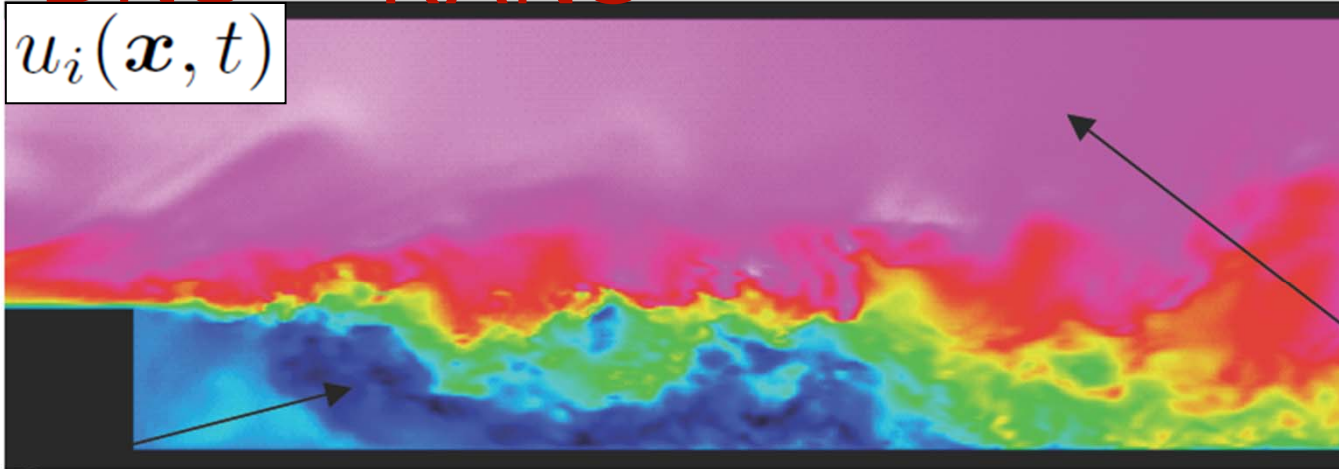
$$K \sim U^2$$

DNS – RANS

DNS

Istantaneous

$$u_i(x, t)$$



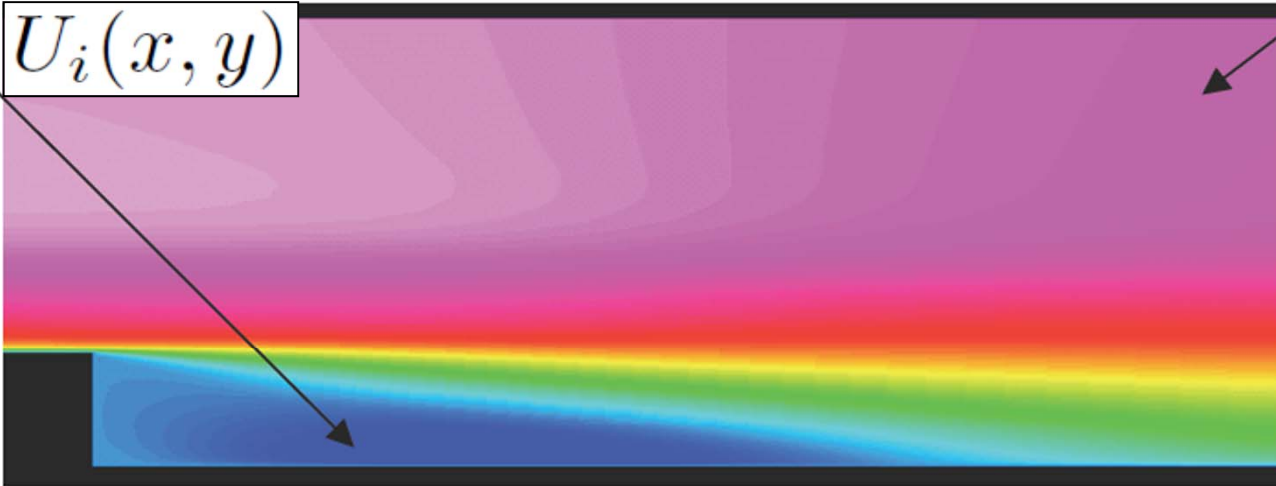
low velocity regions

high velocity regions

RANS

Time averaged

$$U_i(x, y)$$

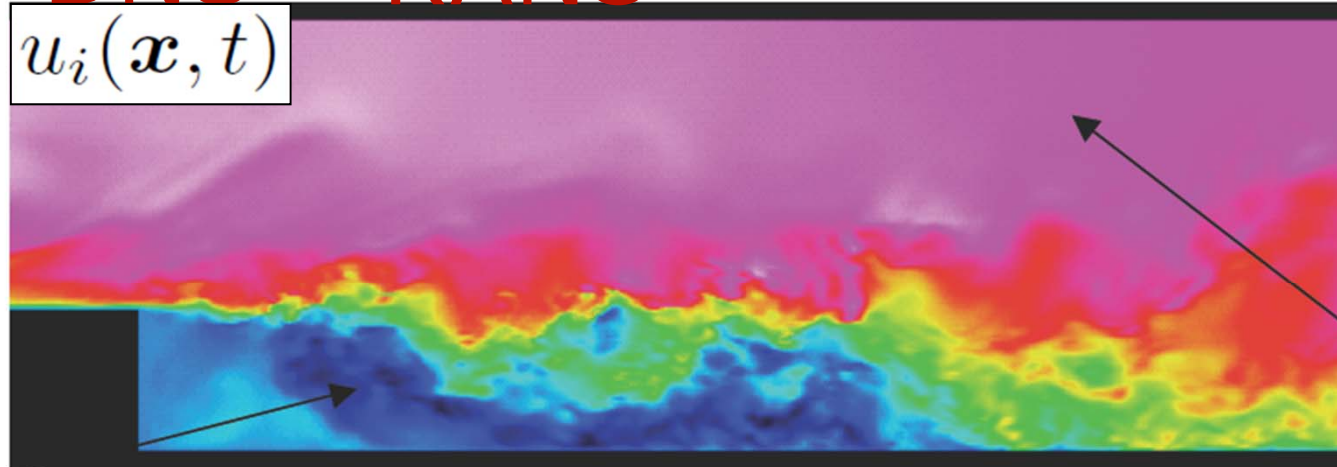


Length of the recirculation region is of engineering interest

DNS – RANS

DNS

Istantaneous



low velocity regions

high velocity regions

DNS (and also LES):

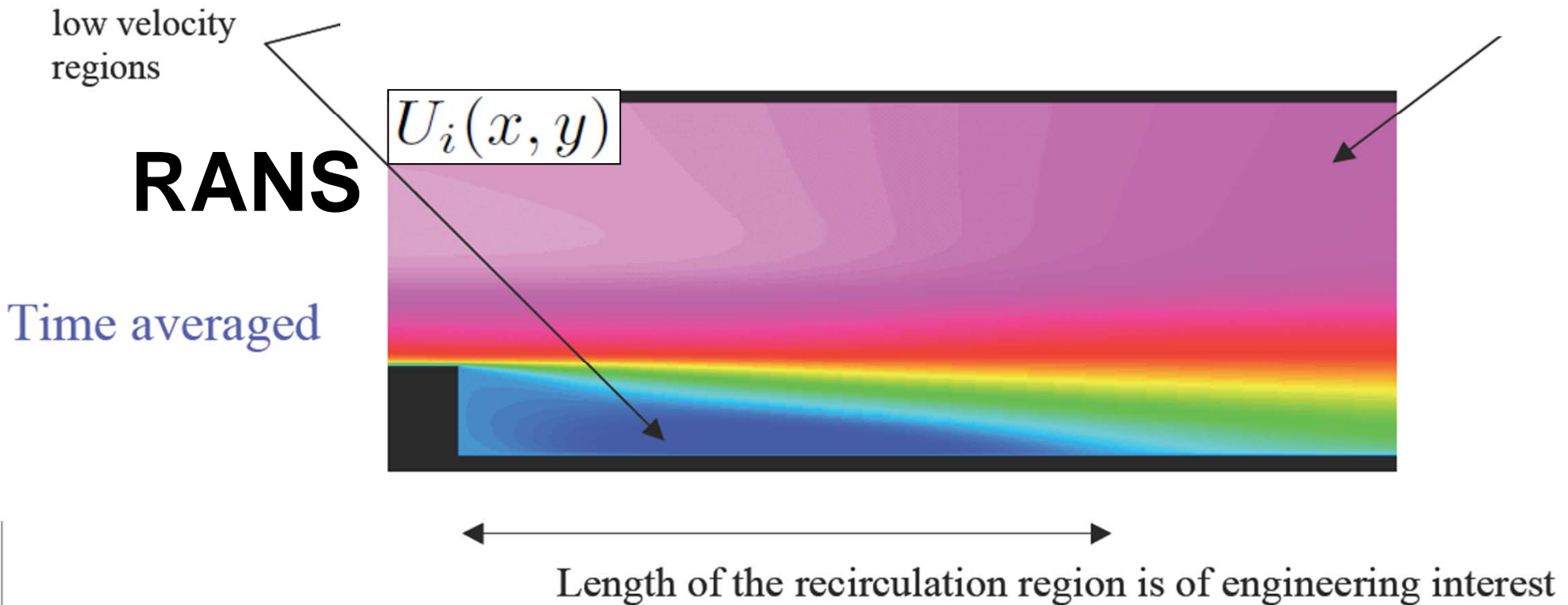
- 3D
- Time dependent
 - Full information of turbulence scales
 - Acoustics and dynamic loads
- Huge Reynolds number dependency

Expensive!

DNS – RANS

RANS:

- Reduction of dimensions → cheap
Here: 2D and steady
- Only statistical information of turbulence scales:
Time and length scales
rms values



Scale separation



- Large scales L and U related to geometrical scales
- Small viscous scales (related to ν and ε)

$$l_K = \eta \sim \left(\frac{\nu^3}{\varepsilon}\right)^{1/4}, \quad t_K \sim \sqrt{\frac{\nu}{\varepsilon}}$$

- Scale separation

$$\frac{L}{\eta} \sim Re^{3/4}, \quad \frac{t}{t_K} \sim Re^{1/2}$$

- Reynolds number

$$Re = \frac{LU}{\nu}$$

Different Reynolds numbers



- Based on global scales

$$Re_L = \frac{LU}{\nu}$$

- Based on distance x from leading edge (flat plate)

$$Re_x = \frac{xU}{\nu}$$

- Based on boundary layer thickness (δ)

$$Re_\delta = \frac{\delta U}{\nu}$$

- Based on wall skin friction

$$Re_\tau = \frac{\delta u_\tau}{\nu}$$

Viscosity

- Kinematic viscosity, ν
- Dynamic viscosity, μ
- Density, ρ

$$\mu = \rho\nu$$



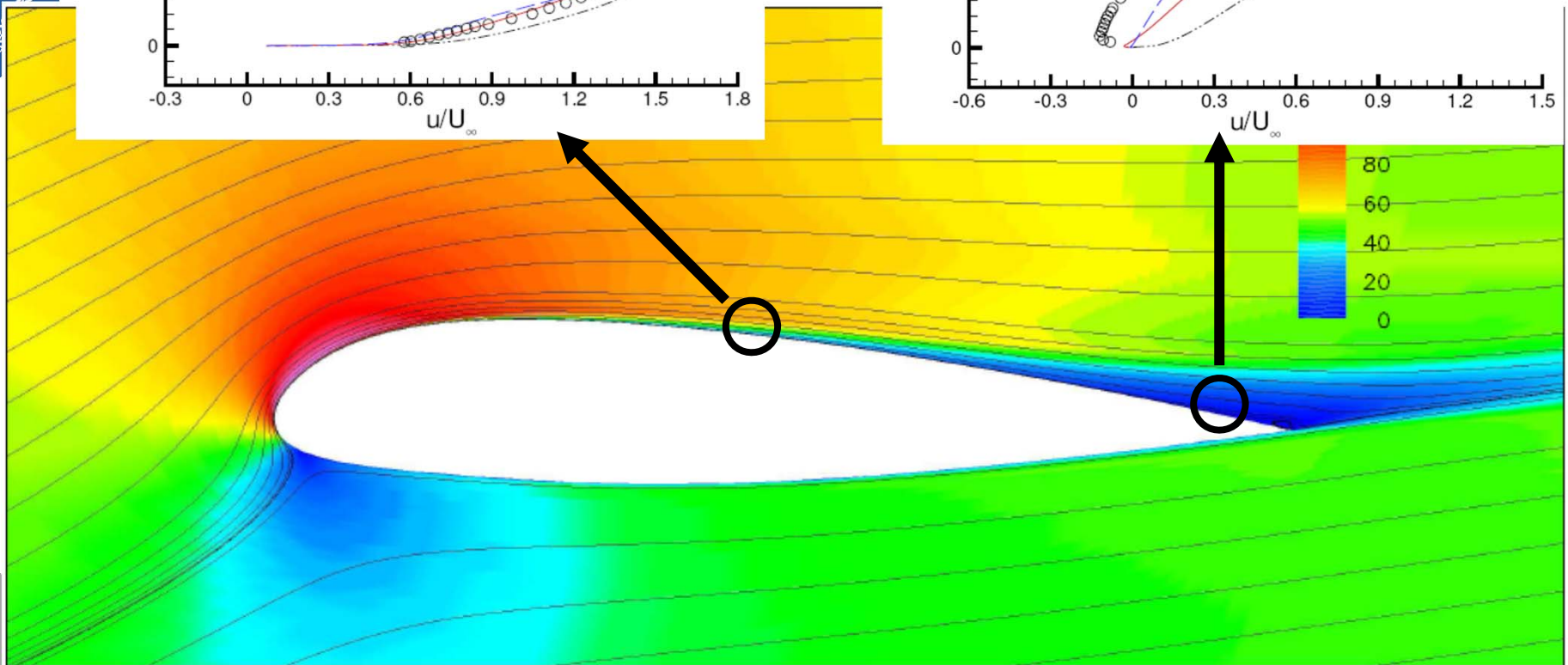
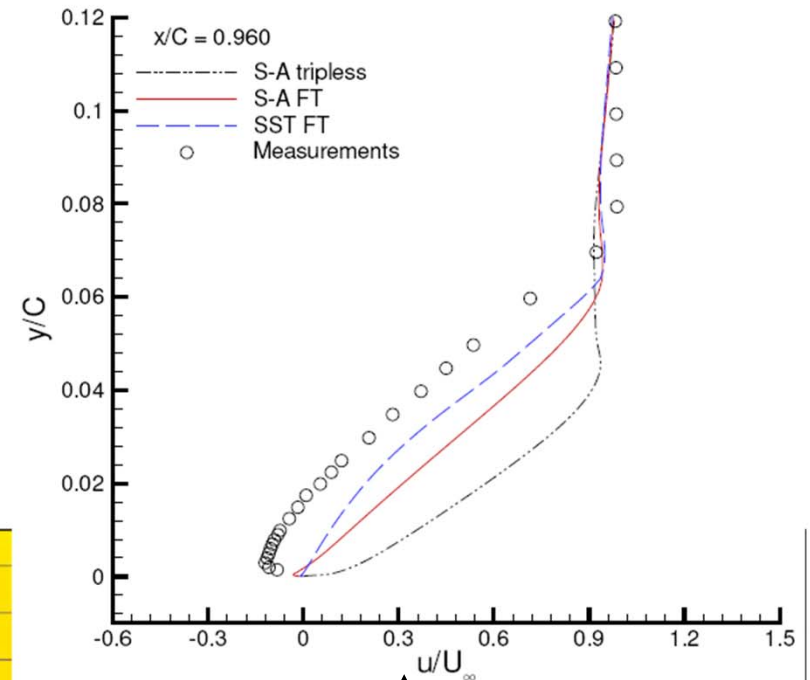
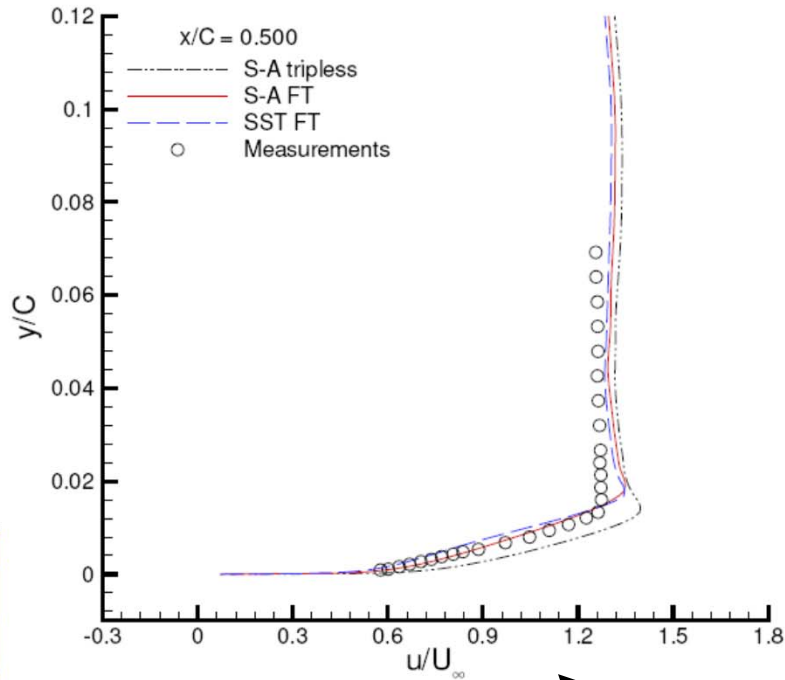
Boundary layers (BL)



- Thin layers
 - Thickness Reynolds number dependent
- Laminar boundary layers
 - Thickness related to wall skin friction
- Turbulent boundary layers
 - Inner and outer scales separated
 - Scale separation Reynolds number dependent

- Figures (Wing+bl – bl – near-wall)

BL on the ONERA A-profile



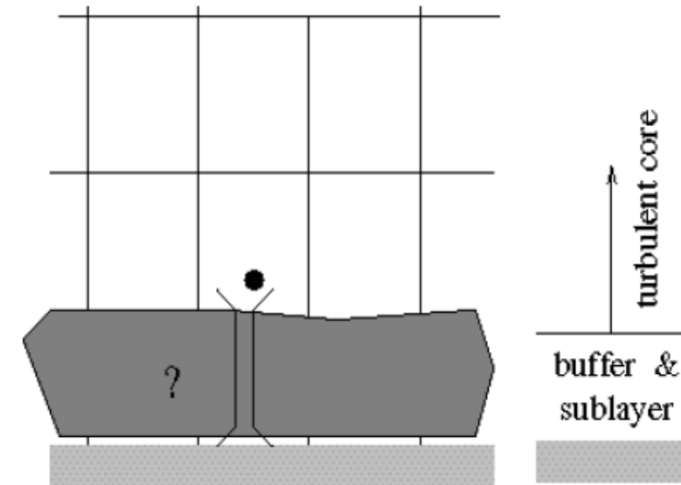
Approximation of BLs



- Slip wall boundary condition
 - Boundary layer completely neglected
 - Euler (non-viscous) computations possible
 - Slip BC can also be applied to viscous & turbulent CFD
- No slip boundary condition
 - Boundary layer completely resolved ($y^+ = 1$)
 - Extreme resolution needed ($\Delta y = 1-100\mu\text{m}$)
 - 40-80 grid points within the boundary layer
- Log-law boundary condition (turbulence)
 - First grid point within log layer ($y^+ > 20$ AND $y < 0.1\delta$)
 - 10-20 grid points within the boundary layer
 - Warning: standard log-law BCs inconsistent with too small grid size. READ SOLVER DOCUMENTATION !!!

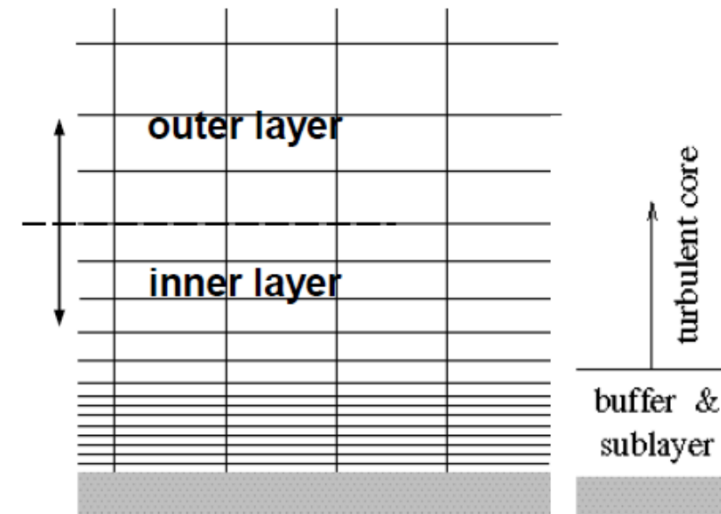
What's in Fluent?

- Standard and Non-Equilibrium Wall Functions:
 - “Wall adjacent cells should have y^+ values between 30 and 300–500” – (remember $y < 0.1\delta!$)
 - “The mesh expansion ratio should be small (no larger than around 1.2)”
 - “Non-equilibrium wall function method attempts to improve the results for flows with higher pressure gradients, separations, reattachment and stagnation”
- Scalable Wall Functions:
 - Consistent for all y^+ values



What's in Fluent? ...

- Enhanced Wall Treatment Option
 - Combines a blended law-of-the wall and a two-layer zonal model.
 - Suitable for low-Re flows or flows with complex near-wall phenomena.
 - Generally requires a fine near-wall mesh capable of resolving the viscous sublayer
 - $y^+ < 5$, and a minimum of 10–15 cells across the “inner layer” for best results
 - Valid for all y^+
 - Available for all k-e and k-w models
 - Not yet for Spalart-Allmaras ($y^+ < 3$ OR $y^+ > 15$)



Recommendations for Fluent

- For $K-\varepsilon$ models
 - use Enhanced Wall Treatment: EWT- ε
- If wall functions are favored with $K-\varepsilon$ models
 - use scalable wall functions
- For $K-\omega$ models
 - use the default: EWT- ω



Wall bounded turbulence

- Viscous wall scales

$$l_* = \frac{\nu}{u_\tau}, \quad t_* = \frac{\nu}{u_\tau^2}$$

- Wall friction velocity

$$u_\tau = \sqrt{\frac{\tau_w}{\rho}} = \sqrt{\nu \left. \frac{\partial U}{\partial y} \right|_{\text{wall}}} = U \sqrt{\frac{1}{2} C_f}$$

- Friction coefficient

$$C_f = \frac{\tau_w}{\frac{1}{2} \rho U^2} = 2 \left(\frac{u_\tau}{U} \right)^2$$

- Viscous wall distance

$$y^+ = \frac{y}{l_*} = \frac{y u_\tau}{\nu}$$



Empirical relations for BLs



- Friction coefficient

- Turbulent $\frac{C_f}{2} \approx 0,0296 Re_x^{-1/5}$

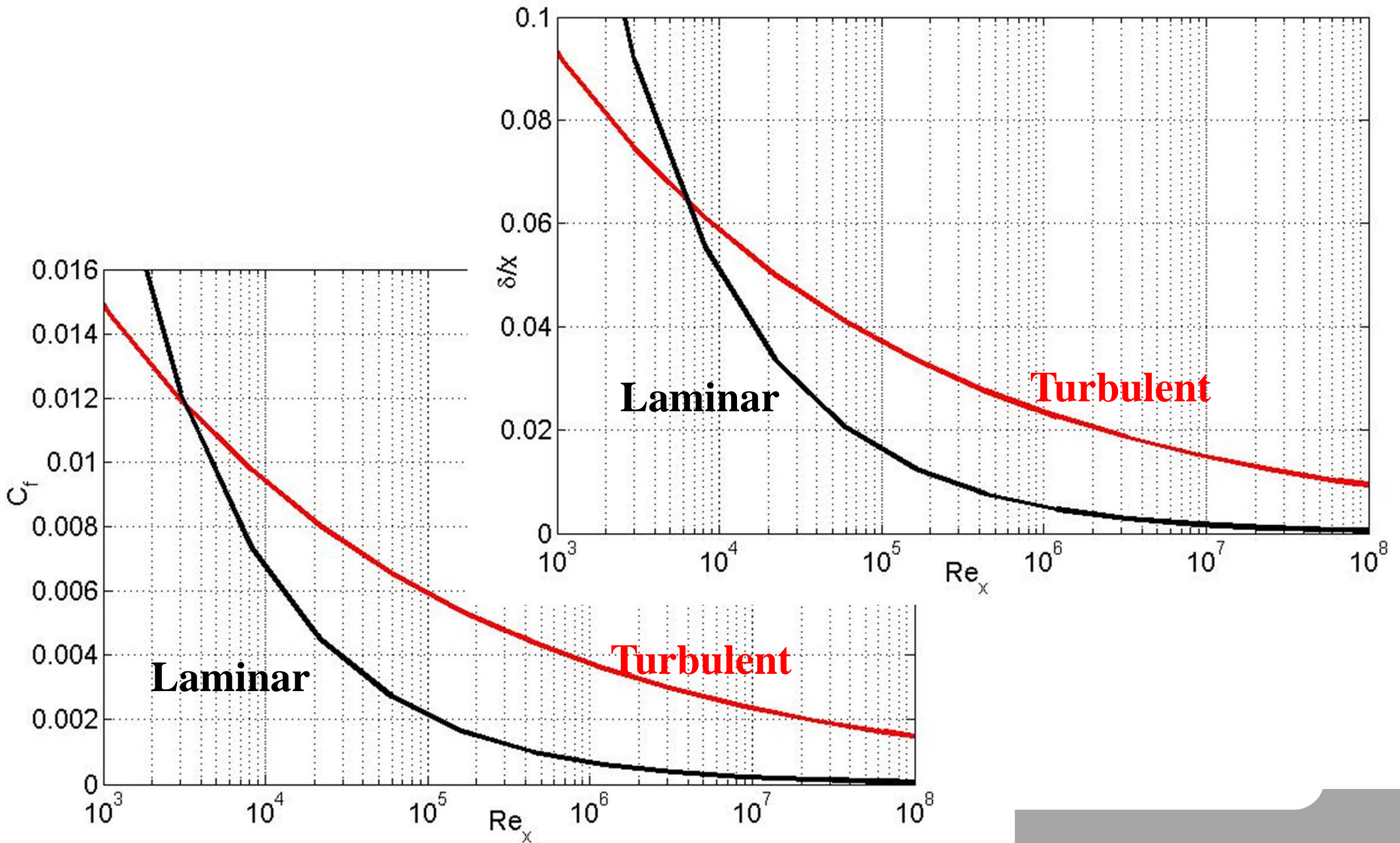
- Laminar $\frac{C_f}{2} = 0,332 Re_x^{-1/2}$

- Boundary layer thickness

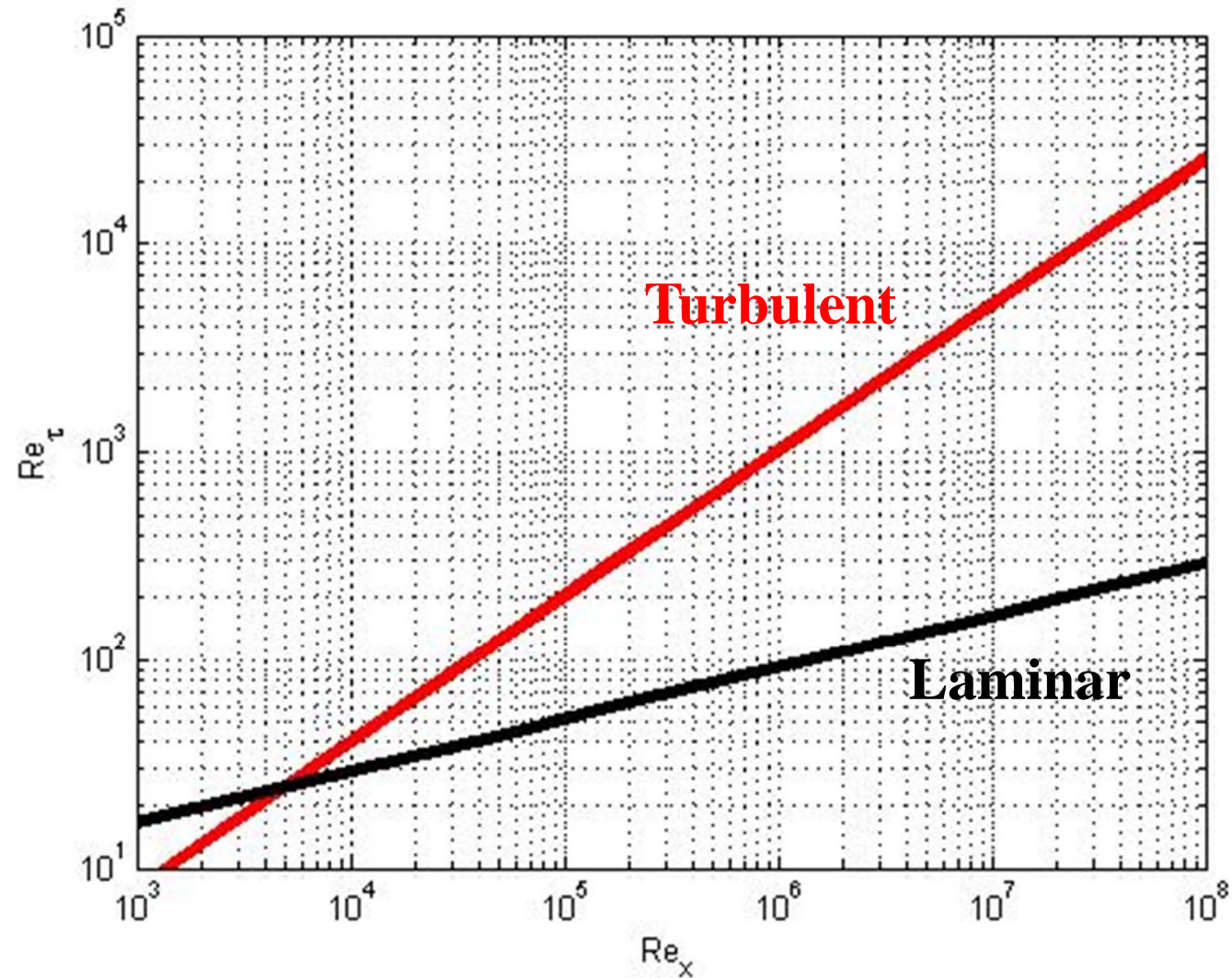
- Turbulent $\frac{\delta}{x} \approx 0,37 Re_x^{-1/5}$

- Laminar $\frac{\delta}{x} = 5,0 Re_x^{-1/2}$

Empirical relations plotted



Empirical relations plotted



Turbulence modelling

- Reynolds decomposition

$$\tilde{u}_i(\mathbf{x}, t) = U_i(\mathbf{x}) + u_i(\mathbf{x}, t)$$

$$\text{where } U_i(\mathbf{x}) = \overline{\tilde{u}_i(\mathbf{x}, t)} \text{ and } \overline{u_i(\mathbf{x}, t)} = 0$$

- The “mean” is time average, ensemble average or averaging in homogeneous directions. $U_i(\mathbf{x})$ may actually vary in time with a time scale much longer than the turbulent time scale.
- Take the mean of the Navier-Stokes equations -> RANS

$$\frac{\partial U_i}{\partial x_i} = 0$$

$$\frac{\partial U_i}{\partial t} + U_k \frac{\partial U_i}{\partial x_k} = -\frac{1}{\rho} \frac{\partial P}{\partial x_i} + \frac{\partial}{\partial x_k} \left(\nu \frac{\partial U_i}{\partial x_k} - \overline{u_i u_k} \right)$$



Reynolds stresses



- Not “small”
- Significant effects on the flow
- Needs to be modelled in terms of mean flow quantities
- Reduces the problem to steady (or slowly varying)
- 2D assumptions possible

- Equation can be derived from Navier-Stokes equations
- Need modelling

Eddy-viscosity models (EVM)

- Assume: Reynolds stresses related to an “eddy viscosity”, ν_T

$$\overline{u_i u_j} = -2\nu_T S_{ij} \quad \left(+ \frac{1}{3} \overline{u_k u_k} \delta_{ij} \right)$$

$$\text{where } S_{ij} = \frac{1}{2} \left(\frac{\partial U_i}{\partial x_j} + \frac{\partial U_j}{\partial x_i} \right)$$

Based on Boussinesq (1877)

- Eddy viscosity \sim turbulence velocity V and length L scales: $\nu_T \sim VL$



One-equation models



- One transport equation for K (turbulent kinetic energy) or ν_T .
- Additional information from global conditions (typically wall distance)
- Works well for attached boundary layers
- Not very general, but more than algebraic models
- Example: Spalart-Allmaras (1992)
 - reasonable and robust model for external aerodynamics
 - Boeing's "standard model"

Two-equation models



- Two transport equations for the turbulence scales ($K-\varepsilon$ or $K-\omega$)
- Completely determined in terms of local quantities (except near-wall corrections which may be dependent on wall distance)
- Works well for attached boundary layers
- Somewhat more general than zero-, one-equation models
- Model transport equations loosely connected to the exact equations.

- Examples:
 - Standard $K-\varepsilon$ model (Launder & Spalding 1974)
 - Wilcox $K-\omega$ (1988, ...) models
 - Menter (1994) SST $K-\omega$ model (performing reasonable well also in separated flows)
 - Airbus' "standard model"

Eddy-viscosity models ...



- Problems:
 - No dependency on rotation or curvature. Real turbulence strongly dependent.
 - Modelled production proportional to strain rate squared $\sim S^2$. Exact production $\sim S$. Results in a overestimated production of K in highly sheared flows (around stagnation points, impinging jets, pressure gradient BLs, separated flows).
- Fixes
 - Rotation & curvature corrections
 - Yap correction (limit excessive turbulent lengthscale)
 - Menter SST correction (limit excessive v_T).

LES and LES/RANS hybrids



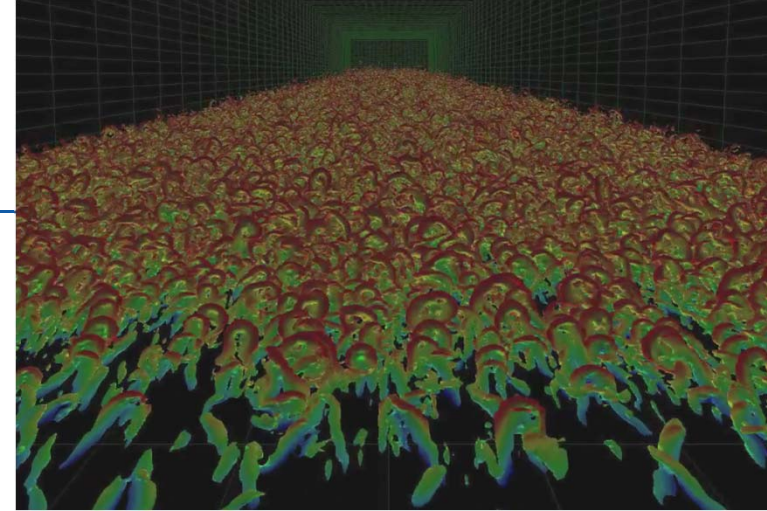
- Simulation of only the large scale turbulence (compare with DNS, simulation of all scales)
 - Always time dependent and 3D -> expensive
- Wall free turbulence simulations almost Re independent
- Wall bounded turbulence largely Re dependent
 - fully resolved near-wall region very expensive (almost as DNS)
 - wall-function or near-wall RANS coupling saves computational cost
 - hybrid RANS-LES (RANS in attached BLs and LES in wall-free separated regions) a very active research field, eg DES

LES and LES/RANS hybrids ...



- LES in academic research for:
 - low Re generic flows
 - complement to DNS for higher Re
 - gives detailed knowledge about turbulence
- LES in industrial use in:
 - internal flow with complex geometries
 - flows around blunt bodies (with large separated regions)
 - atmospheric boundary layers (e.g. weather forecasts)
 - combustion simulation
 - other complex flow physics at moderate Re
- Warning: LES is extremely expensive in high attached and slightly separated wall-bounded flows, if properly resolved.

How expensive is DNS?



- **DNS of flat plate turbulent boundary layer**
 - Schlatter, et al., KTH, Dept. of Mechanics
 - APS meeting 2010: <http://arxiv.org/abs/1010.4000>
 - <http://www.youtube.com/watch?v=4KeaAhVoPIw>
 - <http://www.youtube.com/watch?v=zm9-hSP4s3w>
 - $Re_\theta = 4300$
 - $8192 \times 513 \times 768 = 3.2 \times 10^9$ spectral modes (7.5×10^9 nodes)
 - $\Delta x^+ = 9, \Delta z^+ = 4 \rightarrow$ box: $L^+ = 70\,000, H^+ = W^+ = 3\,000$
 - BL relations: $Re_x = 1.4 \times 10^6$
 - CPU time: 3 months @ 4000 CPU cores = 1 unit
- **DNS of model airplane, same Reynolds number ($Re_x = 1.4 \times 10^6$)**
 - Only a narrow stripe – wing requires about 1 000 stripes
 - $N_{\text{nodes}} = 10^{13}$
 - CPU = 10^3 units

Empirical turbulent BL relations

- **Skin friction coefficient:** $\frac{C_f}{2} = \frac{\tau_w}{\rho U_\infty^2} = \left(\frac{Re_\tau}{Re_\delta} \right)^2 \approx 0.0296 Re_x^{-1/5}$
- **Boundary layer thickness:** $\frac{\delta}{x} = \frac{Re_\delta}{Re_x} \approx 0.37 Re_x^{-1/5}$
- **Boundary layer momentum thickness:** $Re_\tau \approx 1.13 Re_\theta^{0.843}$
- **Reynolds numbers:**
 $Re_\tau \equiv \frac{\delta u_\tau}{\nu}$ $Re_\theta \equiv \frac{\theta U_\infty}{\nu}$ $Re_\delta \equiv \frac{\delta U_\infty}{\nu}$ $Re_x \equiv \frac{x U_\infty}{\nu}$

DNS – full scale airplane

- Re scaling – wall bounded flow

- **Nodes:** $N_{nodes} \sim \frac{L \times B \times H}{\Delta x \Delta z \Delta y} \sim L^{+2} H^{+} \sim Re_x^{5/2}$

- **Time steps:** $N_{\Delta T} \sim \frac{T}{\Delta T} \sim T^{+} \sim Re_x^{4/5}$

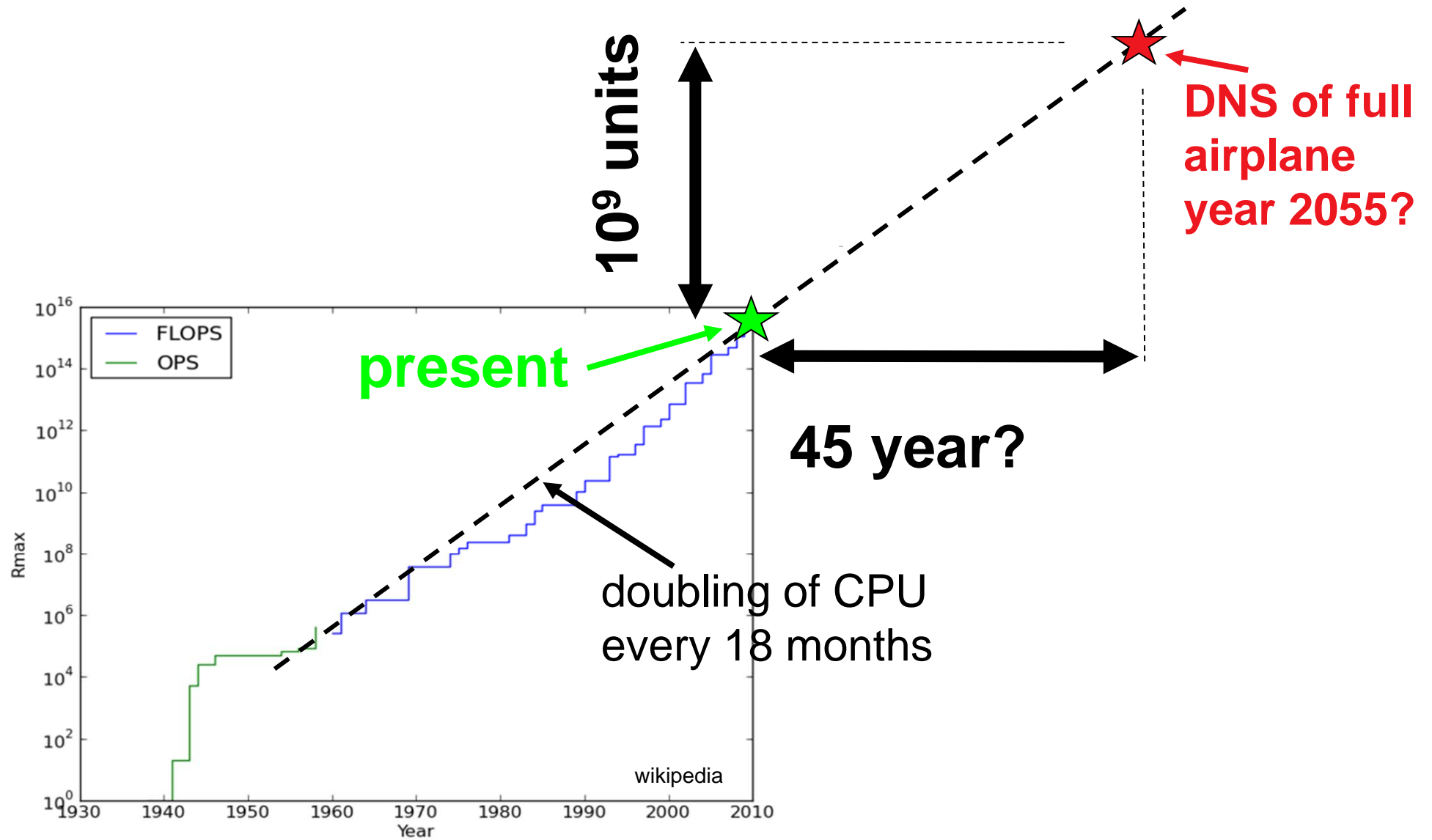
- **CPU time:** $N_{CPU} \sim N_{nodes} \times N_{\Delta T} \sim Re_x^{33/10}$

- DNS of Airplane ($Re_x = 70 \times 10^6$) (factor of 50)

- $N_{nodes} = 10^{17}$

- CPU = 10^9 units

Supercomputer development



Computational effort – different approaches

Name	Aim	Unsteady	<i>Re</i> -dependence	3/2D	Empiricism	Grid	Steps	Ready
2DURANS	Numerical	Yes	Weak	No	Strong	10^5	$10^{3.5}$	1980
3DRANS	Numerical	No	Weak	No	Strong	10^7	10^3	1990
3DURANS	Numerical	Yes	Weak	No	Strong	10^7	$10^{3.5}$	1995
DES	Hybrid	Yes	Weak	Yes	Strong	10^8	10^4	2000
LES	Hybrid	Yes	Weak	Yes	Weak	$10^{11.5}$	$10^{6.7}$	2045
QDNS	Physical	Yes	Strong	Yes	Weak	10^{15}	$10^{7.3}$	2070
DNS	Numerical	Yes	Strong	Yes	None	10^{16}	$10^{7.7}$	2080

From Spalart, Int. J. Heat and Fluid Flow, 2000

- **RANS: Reynolds Averaged Navier-Stokes**
- **URANS: Unsteady RANS – slowly in time**
- **DES: Detached Eddy Simulation**
- **LES: Large eddy simulation**
- **QDNS: Quasi DNS, or wall resolved LES**
- **DNS: Direct Numerical Simulation (of the Navier-Stokes eq's)**
- **“Ready”**: When first results can be expected